

Page	Correction	Page	Correction
44	Equation (2.2) should be <u>sugar recovered</u> not sucrose recovered [consistent with eq (2.1)].	152	Equation (6.10) should read: $\dot{V}_L = b \cdot l \cdot u_{0,L} \quad (6.10)$
44	Equation (2.3) should read: $\text{sugar recovered} = \frac{9600 \cdot (P_J - 30)}{P_J \cdot (P_S - 30)} \% \quad (2.3)$	157	Equation (6.15) should read: $F = g \cdot \mu \cdot (m + m_{\text{chain}}) / 1000 \quad (6.15)$ where m is the mass of fiber <u>in kg</u> and juice ...
93	Left column, 11 th line from the bottom: ... Where cane is harvested mechanically and delivered in billets, this problem is <u>minimized</u> and inserts are used with success. ...	205	Equation (9.18): the units for the heat transfer coefficient k should be $W/(m^2 \cdot K) \text{ [not } kW/(m^2 \cdot K)]$
94	3 rd line below Figure 4.10: ... Rotor construction on heavy duty shredders is massive and the <u>moment of inertia</u> of the rotor is generally high enough so that the need for a flywheel is eliminated. ...	233	Equation (10.9) should read: $u_t = \frac{g \cdot (\rho_p - \rho_j) \cdot d_p^2}{18 \cdot \mu} \quad (10.9)$
107	Left column, 4 th to 7 th line of that page: <ul style="list-style-type: none">• For a mill with rolls turning at 3 min⁻¹, absorbed torque is thus <u>20 to 30</u> kN · m per t fiber/h.• For a mill with rolls turning at 5 min⁻¹, the absorbed torque is <u>12 to 18</u> kN · m per t fiber/h.	254	Figure 11.9: Photo has been inverted and rotated 90°.
130 / 131	The values given in the last colored row of Table 5.6 for Brix of juice in % are incorrect, as they do not allow for Brix-free water. The correct values are: 19.8 19.7 20.0 10.5 9.1 14.1 7.0 5.6 10.9 4.3 3.1 7.6 2.2 1.3 5.6 0.0 13.8 13.8	297	Section 12.7.3, 2 nd sentence: ... The downtake is around 40% of the diameter of the pan, but in Robert type evaporator the downtakes comprise a much smaller proportion of the cross sectional area, less than 25% of the <u>diameter</u>
139	Figure 5.25: Extra zero has been added to mill widths on each line. Mill widths should be <u>1400</u> (not 14000), <u>1275</u> (not 12750), <u>1180</u> , <u>1100</u> , <u>1020</u> , <u>950</u> , <u>870</u> and <u>780</u> .	319	Table 13.1, 4 th column, 4 th value from bottom: substitute <u>673</u> for 716 mm Hg.
151	Right column, last sentence: replace “ith stage” with “(i+1)th stage”. The sentence should read: ... Thus for liquid pumped from the (i+1)th stage to exit in the ith stage, the spray or weir should be positioned a distance l_A from the middle of the (i+1)th stage, where the spray advance l_A is given by: ...	321	Last sentence in Section 13.1.2: $(t_{VS} - t_o)$ [not $(t_o - t_{VS})$].
		377	Equation (15.35), units of n: s ⁻¹ (not min ⁻¹)
		377	Right column, last sentence at the bottom of page: ... The effective viscosity μ_{eff} is used in this formula and is based on the average shear rate, <u>which is</u> suggested to be about $11 \cdot n$, ...
		501	Table 21.4: Heading of middle column should be: <u>Molasses apparent purity</u> .

Page Correction

514 Section 22.2.4, right column, at the end of 2nd para: The terminal settling velocity ... is < 0.01 m/s (not < 0.1 m/s).

528 Right column, 2nd last line: ... (Section 17.3.6) not (Section 17.4.6).

587 Section 25.3.3, Filter cake loss, 3rd line from the bottom should be:
... between 0.2 and 5 kg/100 kg sucrose ...

590 Equation (25.19): should be 5670 (not 5760).

609 2nd para, 3rd line: ... temperature of the gas ... must be kept above the dew point ...

621 Equation (27.2): the first term should be 18 260 (not 182 60).

663 Figure 27.28, X-axis: first two numbers should be 50 and 100, not 60 and 60.

677 Figure 28.5: HP steam range pressure (right, 2nd from the top) should be 6.1 MPa (not 3.1).

680 Section 29.1.2, 8th line: ... drift loss should be 0.05 % of the water flow ... (not 5 %).

739 Equation 32.4, third term: replace 258.5 by $2.585 \cdot 10^{-4} \cdot t^2$.

744 Equation (32.12) should read:

$$\lambda = \left[0.561 + 0.206 \cdot \left(\frac{t}{100} \right) - 0.0943 \cdot \left(\frac{t}{100} \right)^2 - 0.007746 \cdot \left(\frac{t}{100} \right)^3 \right] \cdot \left[1 - 0.54 \cdot \left(\frac{w_{DS}}{100} \right) \right] \quad (32.12)$$

747 Equation (32.18) should read:

$$c_{CaO} = 8.611 \cdot \text{°Baumé} + 0.0827 \cdot \text{°Baumé}^2.$$