

Page	Correction	Page	Correction
44	Equation (2.2) should be <u>sugar recovered</u> not sucrose recovered [consistent with eq (2.1)].	152	Equation (6.10) should read: $\dot{V}_L = b \cdot l \cdot u_{0,L} \quad (6.10)$
44	Equation (2.3) should read: $\text{sugar recovered} = \frac{9600 \cdot (P_J - 30)}{P_J \cdot (P_S - 30)} \% \quad (2.3)$	157	Equation (6.15) should read: $F = g \cdot \mu \cdot (m + m_{\text{chain}}) / 1000 \quad (6.15)$ where $m$ is the mass of fiber and juice in kg <u>in</u> kg and juice ...
93	Left column, 11 <sup>th</sup> line from the bottom: ... Where cane is harvested mechanically and delivered in billets, this problem is <u>minimized</u> and inserts are used with success. ...	205	Equation (9.18): the units for the heat transfer coefficient $k$ should be $\text{W}/(\text{m}^2 \cdot \text{K}) \text{ [not kW}/(\text{m}^2 \cdot \text{K})]$
94	3 <sup>rd</sup> line below Figure 4.10: ... Rotor construction on heavy duty shredders is massive and the <u>moment of inertia</u> of the rotor is generally high enough so that the need for a flywheel is eliminated. ...	233	Equation (10.9) should read: $u_t = \frac{g \cdot (\rho_P - \rho_J) \cdot d_p^2}{18 \cdot \mu} \quad (10.9)$
107	Left column, 4 <sup>th</sup> to 7 <sup>th</sup> line of that page: <ul style="list-style-type: none"><li>• For a mill with rolls turning at 3 min<sup>-1</sup>, absorbed torque is thus <u>20 to 30</u> kN · m per t fiber/h.</li><li>• For a mill with rolls turning at 5 min<sup>-1</sup>, the absorbed torque is <u>12 to 18</u> kN · m per t fiber/h.</li></ul>	254	<b>Figure 11.9:</b> Photo has been inverted and rotated 90°.
130 / 131	The values given in the last colored row of <b>Table 5.6</b> for Brix of juice in % are incorrect, as they do not allow for Brix-free water. The correct values are: 19.8   19.7   20.0   10.5   9.1   14.1 7.0   5.6   10.9   4.3   3.1   7.6 2.2   1.3   5.6   0.0   13.8   13.8	281	Equation 12.37 should read: $\dot{m}_{\text{FV},i} = \dot{m}_{\text{C},i} \cdot \frac{h_{\text{C},i} - h_{\text{C},i0}}{\Delta h_{\text{VL},i}} \quad (12.37)$
139	<b>Figure 5.25:</b> Extra zero has been added to mill widths on each line. Mill widths should be <u>1400</u> (not 14000), <u>1275</u> (not 12750), <u>1180</u> , <u>1100</u> , <u>1020</u> , <u>950</u> , <u>870</u> and <u>780</u> .	297	Section 12.7.3, 2 <sup>nd</sup> sentence: ... The downtake is around 40 % of the diameter of the pan, but in <i>Robert</i> type evaporators the downtakes comprise a much smaller proportion of the cross sectional area, less than 25 % of the <u>diameter</u> . ...
151	Right column, last sentence: replace “ $i$ th stage” with “ $(i+1)$ th stage”. The sentence should read: ... Thus for liquid pumped from the $(i+1)$ th stage to exit in the $i$ th stage, the spray or weir should be positioned a distance $l_A$ from the middle of the <u><math>(i+1)</math>th</u> stage, where the spray advance $l_A$ is given by: ...	319	<b>Table 13.1</b> , 4 <sup>th</sup> column, 4 <sup>th</sup> value from bottom: substitute <u>673</u> for 716 mm Hg.
		321	Last sentence in Section 13.1.2: $(t_{\text{VS}} - t_0) \text{ [not } (t_0 - t_{\text{VS}})].$
		377	Equation (15.35), units of $n$ : s <sup>-1</sup> (not min <sup>-1</sup> )

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| 377  | Right column, last sentence at the bottom of page:<br>... The effective viscosity $\mu_{\text{eff}}$ is used in this formula and is based on the average shear rate, <u>which is</u> suggested to be about $11 \cdot n$ , ... |
| 501  | <b>Table 21.4:</b> Heading of middle column should be: <u>Molasses apparent purity</u> .  |
| 514  | Section 22.2.4, right column, at the end of 2 <sup>nd</sup> para: The terminal settling velocity ... is <u>&lt; 0.01 m/s</u> (not < 0.1 m/s).   |
| 528  | Right column, 2 <sup>nd</sup> last line: ... (Section <u>17.3.6</u> ) not (Section 17.4.6).   |
| 587  | Section 25.3.3, <b>Filter cake loss</b> , 3 <sup>rd</sup> line from the bottom should be:<br>... between <u>0.2 and 5 kg/100 kg</u> sucrose ...   |
| 590  | Equation (25.19): should be <u>5670</u> (not 5760).   |
| 609  | 2 <sup>nd</sup> para, 3 <sup>rd</sup> line: ... temperature of the gas ... must be kept <u>above</u> the dew point ...  |
| 621  | Equation (27.2): the first term should be 18 260 (not 182 60).  |
| 663  | <b>Figure 27.28</b> , X-axis: first two numbers should be <u>50</u> and <u>100</u> , not 60 and 60.   |
| 677  | <b>Figure 28.5:</b> HP steam range pressure (right, 2 <sup>nd</sup> from the top) should be <u>6.1 MPa</u> (not 3.1).   |
| 680  | Section 29.1.2, 8 <sup>th</sup> line: ... drift loss should be <u>0.05 %</u> of the water flow ... (not 5 %).   |
| 739  | Equation 32.4, third term: replace 258.5 by <u><math>2.585 \cdot 10^{-4} \cdot t^2</math></u> .   |
| 744  | Equation (32.12) should read:   |

$$\lambda = \left[ 0.561 + 0.206 \cdot \left( \frac{t}{100} \right) - 0.0943 \cdot \left( \frac{t}{100} \right)^2 - 0.007746 \cdot \left( \frac{t}{100} \right)^3 \right] \cdot \left[ 1 - 0.54 \cdot \left( \frac{w_{\text{DS}}}{100} \right) \right] \quad (32.12)$$

- 747 Equation (32.18) should read:  
 $c_{\text{CaO}} = 8.611 \cdot \text{°Baumé} + 0.0827 \cdot \text{°Baumé}^2$ .